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NEWS	2		"Ask CAS" for self-help around the clock
NEWS	3	AUG 09	INSPEC enhanced with 1898-1968 archive
NEWS	4	AUG 28	ADISCTI Reloaded and Enhanced
NEWS	5	AUG 30	CA(SM)/CAPLUS(SM) Austrian patent law changes
NEWS	6	SEP 21	CA/CAPLUS fields enhanced with simultaneous left and right truncation
NEWS	7	SEP 25	CA(SM)/CAPLUS(SM) display of CA Lexicon enhanced
NEWS	8	SEP 25	CAS REGISTRY(SM) no longer includes Concord 3D coordinates
NEWS	9	SEP 25	CAS REGISTRY(SM) updated with amino acid codes for pyrrolysine
NEWS	10	SEP 28	CEABA-VTB classification code fields reloaded with new classification scheme
NEWS	11	OCT 19	LOGOFF HOLD duration extended to 120 minutes
NEWS	12	OCT 19	E-mail format enhanced
NEWS	13	OCT 23	Option to turn off MARPAT highlighting enhancements available
NEWS	14	OCT 23	CAS Registry Number crossover limit increased to 300,000 in multiple databases
NEWS	15	OCT 23	The Derwent World Patents Index suite of databases on STN has been enhanced and reloaded
NEWS	16	OCT 30	CHEMLIST enhanced with new search and display field
NEWS	17	NOV 03	JAPIO enhanced with IPC 8 features and functionality
NEWS	18	NOV 10	CA/CAPLUS F-Term thesaurus enhanced
NEWS	19	NOV 10	STN Express with Discover! free maintenance release Version 8.01c now available
NEWS	20	NOV 20	CAS Registry Number crossover limit increased to 300,000 in additional databases
NEWS	21	NOV 20	CA/CAPLUS to MARPAT accession number crossover limit increased to 50,000
NEWS	22	DEC 01	CAS REGISTRY updated with new ambiguity codes
NEWS	23	DEC 11	CAS REGISTRY chemical nomenclature enhanced
NEWS	24	DEC 14	WPIDS/WPINDEX/WPIX manual codes updated
NEWS	25	DEC 14	GBFULL and FRFULL enhanced with IPC 8 features and functionality
NEWS	26	DEC 18	CA/CAPLUS pre-1967 chemical substance index entries enhanced with preparation role
NEWS	27	DEC 18	CA/CAPLUS patent kind codes updated
NEWS	28	DEC 18	MARPAT to CA/CAPLUS accession number crossover limit increased to 50,000
NEWS	29	DEC 18	MEDLINE updated in preparation for 2007 reload
NEWS	30	DEC 27	CA/CAPLUS enhanced with more pre-1907 records
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FILE LAST UPDATED: 3 Jan 2007 (20070103/ED)

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=> s cataly? (2a) steam (2a) reform? (p) autothermal (p) series

1354545 CATALY?

210743 STEAM

493 STEAMS

211101 STEAM

(STEAM OR STEAMS)

49993 REFORM?

1332 AUTOTHERMAL

567076 SERIES

9 SERIESES

567082 SERIES

(SERIES OR SERIESES)

L1 4 CATALY? (2A) STEAM (2A) REFORM? (P) AUTOTHERMAL (P) SERIES

=> s l1 ibib ab 1-4

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The search profile that was entered contains terms or nested terms that are not separated by a logical operator.

=> d l1 ibib ab 1-4

L1 ANSWER 1 OF 4 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 2004:269876 CAPLUS
DOCUMENT NUMBER: 140:289193
TITLE: Process for the production of synthesis gas by the
steam reforming of a hydrocarbon feed
INVENTOR(S): Aasberg-Petersen, Kim; Dybkjter, Ib; Christensen,
Peter Seier; Rostrup-Nielsen, Thomas; Erikstrup,
Niels; Hansen, Jetts-Henrik Bak
PATENT ASSIGNEE(S): Den.
SOURCE: U.S. Pat. Appl. Publ., 13 pp.
CODEN: USXXCO
DOCUMENT TYPE: Patent
LANGUAGE: English
FAMILY ACC. NUM. COUNT: 1
PATENT INFORMATION:

PATENT NO.	KIND.	DATE	APPLICATION NO.	DATE
US 2004063797	A1	20040401	US 2003-667389	20030923
EP 1413547	A1	20040428	EP 2003-20673	20030911
R: AT, BE, CH, DE, DK, ES, FR, GB, GR, IT, LI, LU, NL, SE, MC, PT, IE, SI, LT, LV, FI, RO, MK, CY, AL, TR, BG, CZ, EE, HU, SK				
JP 2004149406	A	20040527	JP 2003-331066	20030924
CA 2442491	A1	20040326	CA 2003-2442491	20030925
NO 2003004285	A	20040329	NO 2003-4285	20030925
AU 2003248389	A1	20040422	AU 2003-248389	20030925
ZA 2003007450	A	20040706	ZA 2003-7450	20030925
KR 2004027440	A	20040401	KR 2003-66831	20030926
CN 1498850	A	20040526	CN 2003-164880	20030926
PRIORITY APPLN. INFO.:			DK 2002-1435	A 20020926

AB A process and system for the production of synthesis gas (i.e., H₂-CO mixts.) from a hydrocarbon feed (e.g., natural gas) comprises endothermic and/or adiabatic catalytic steam reforming and autothermal steam reforming in series, where the steam reforming is carried out in one or more endothermic stages in series or in one or more adiabatic steam reforming stages in series with intermediate heating of the feed stock gas leaving the adiabatic reforming stages and where the carbon monoxide-containing gas, characterized by having a molar ratio of hydrogen to carbon of less than 4.5, is added prior to at least one of the endothermic or adiabatic steam reforming stages and/or prior to the autothermal steam reforming step. Process flow diagrams are presented.

L1 ANSWER 2 OF 4 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 2004:260992 CAPLUS
DOCUMENT NUMBER: 140:256073
TITLE: Production of synthesis gas by autothermal steam
reforming
INVENTOR(S): Erikstrup, Niels; Bak Hansen, Jens-Henrik;
Rostrup-Nielsen, Thomas; Dybkjaer, Ib; Christensen,
Peter Seier; Aasberg-Petersen, Kim
PATENT ASSIGNEE(S): Haldor Topsoe A/S, Den.
SOURCE: Eur. Pat. Appl., 14 pp.
CODEN: EPXXDW
DOCUMENT TYPE: Patent
LANGUAGE: English
FAMILY ACC. NUM. COUNT: 1
PATENT INFORMATION:

PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
EP 1403216	A1	20040331	EP 2003-20677	20030911
R: AT, BE, CH, DE, DK, ES, FR, GB, GR, IT, LI, LU, NL, SE, MC, PT,				

IE, SI, LT, LV, FI, RO, MK, CY, AL, TR, BG, CZ, EE, HU, SK

JP 2004269343	A	20040930	JP 2003-329354	20030922
CA 2442770	A1	20040326	CA 2003-2442770	20030925
NO 2003004284	A	20040329	NO 2003-4284	20030925
US 2004063798	A1	20040401	US 2003-669375	20030925
US 7074347	B2	20060711		
AU 2003248393	A1	20040422	AU 2003-248393	20030925
ZA 2003007447	A	20040701	ZA 2003-7447	20030925
KR 2004027448	A	20040401	KR 2003-66872	20030926
CN 1496954	A	20040519	CN 2003-164881	20030926
PRIORITY APPLN. INFO.:			DK 2002-1433	A 20020926
			DK 2002-1434	A 20020926

AB Synthesis gas is produced by catalytic steam reforming of a hydrocarbon containing feedstock in parallel in an autothermal steam reformer and in at least one steam reformer in series, the heat for the steam reforming reactions in the steam reformers being provided by indirect heat exchange with the combined effluents from the steam reformers with the autothermal steam reformer, and wherein carbon monoxide containing gas is added to the feedstock prior to the steam reforming in the autothermal steam reformer and/or prior to the steam reforming in the steam reformers, the CO containing gas having a molar ratio of hydrogen to carbon of <4.5 and being added in an amount resulting in a product stream having a molar ratio of hydrogen to CO of 1.8-2.3. The steam reforming catalyst of a 2st reformer contains Ni and the catalyst of a last steam reformer contains a noble metal. The oxidant of the autothermal steam reformer contains ≥ 90 volume% of oxygen. The CO containing gas is tail gas from a Fischer-Tropsch process.

REFERENCE COUNT: 4 THERE ARE 4 CITED REFERENCES AVAILABLE FOR THIS RECORD. ALL CITATIONS AVAILABLE IN THE RE FORMAT

L1 ANSWER 3 OF 4 CAPLUS COPYRIGHT 2007 ACS on STN
 ACCESSION NUMBER: 2000:160979 CAPLUS
 DOCUMENT NUMBER: 132:196415
 TITLE: Process and reactor system for manufacture of synthesis gas
 INVENTOR(S): Dybkjaer, Ib
 PATENT ASSIGNEE(S): Haldor Topsoe A/S, Den.
 SOURCE: Eur. Pat. Appl., 4 pp.
 CODEN: EPXXDW
 DOCUMENT TYPE: Patent
 LANGUAGE: English
 FAMILY ACC. NUM. COUNT: 1
 PATENT INFORMATION:

PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
EP 983963	A2	20000308	EP 1999-114335	19990721
EP 983963	A3	20001004		
R: AT, BE, CH, DE, DK, ES, FR, GB, GR, IT, LI, LU, NL, SE, MC, PT, IE, SI, LT, LV, FI, RO				
DK 9801098	A	20000302	DK 1998-1098	19980901
DK 173742	B1	20010827		
NO 9904029	A	20000304	NO 1999-4029	19990820
NZ 337468	A	20010126	NZ 1999-337468	19990826
ZA 9905562	A	20001003	ZA 1999-5562	19990830
US 6224789	B1	20010501	US 1999-385724	19990830
CN 1246441	A	20000308	CN 1999-118408	19990831
CN 1124226	B	20031015		
AU 9944887	A1	20000316	AU 1999-44887	19990831
AU 753603	B2	20021024		
JP 2000185906	A	20000704	JP 1999-245109	19990831
PRIORITY APPLN. INFO.:			DK 1998-1098	A 19980901

AB A process is disclosed for production of H₂- and/or CO-rich synthesis gas from

a hydrocarbon feed by catalytic steam reforming. A 1st stream of the feedstock is autothermally steam reformed in parallel with a 2nd stream of the feedstock which is steam reformed in the presence of a fixed-bed steam-reforming catalyst in a heat-conducting relation with a hot effluent from the autothermal steam reforming and with a steam-reformed hot effluent withdrawn from the steam-reforming catalyst. The effluent from the autothermal steam-reforming step and the heat-exchange steam-reforming step are combined after supplying heat to steam-reforming reactions proceeding in the 2nd stream of the feedstock. A reactor system comprises an autothermal reforming reactor and a heat-exchange reactor connected in parallel at inlet side of the reactors and connected in series at an outlet side of the autothermal reactor.

L1 ANSWER 4 OF 4 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 1985:473911 CAPLUS

DOCUMENT NUMBER: 103:73911

TITLE: Fuel cell electric power production

INVENTOR(S): Hwang, Herng Shinn; Heck, Ronald M.; Yarrington, Robert M.

PATENT ASSIGNEE(S): Engelhard Corp., USA

SOURCE: U.S., 14 pp. Cont. of U.S. Ser. No. 430,455 abandoned
CODEN: USXXAM

DOCUMENT TYPE: Patent

LANGUAGE: English

FAMILY ACC. NUM. COUNT: 1

PATENT INFORMATION:

PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
US 4522894	A	19850611	US 1984-599865	19840413
PRIORITY APPLN. INFO.:			US 1982-430455	A1 19820930

AB In fuel-cell power generation a H-rich fuel is generated by treating a hydrocarbon feed in an autothermal reformer using a 1st monolithic catalyst zone having Pd and Pt catalytic components and a 2nd Pt-group metal steam-reforming catalyst. Air is used as the oxidant in the hydrocarbon reforming zone and a low O:C ratio is maintained to control the amount of dilution of the H-rich gas with N of the air without sustaining an insupportable amount of C deposition on the catalyst. Anode vent gas may be used as the fuel to preheat the inlet stream to the reformer. The fuel cell and the reformer are preferably operated at elevated pressures, .ltorsim.150 psia for the fuel cell. Thus, a series of Pt-Pd partial oxidation monolithic catalyst compns. was prepared Generally, as the S content of the hydrocarbon feed being treated in the 1st catalyst zone increases, a higher Pt:Pd ratio is preferred. The reverse is true for feeds with relatively high CH4 content. The steam-reforming catalyst may use a monolithic or a particulate (spheres, extrudates, granules, shaped members) support. The use of the Pt-Rh steam-reforming catalyst attained an .apprx.100% conversion of the Number 2 fuel oil vs. 96.7% when the Ni catalyst was used. When Ni catalyst was used, a rapid increase in the reactor pressure drop was observed